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PHOTOCATALYTIC GENERATION OF HYDROGEN FROM HYDROGEN SULFIDE: AN ENERGY BARGAIN*

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Abstract—The current energy crisis has led to the high priority of solar energy related research. Conversion of solar energy into chemical fuels has attained great importance. The generation of hydrogen with solar energy from inexpensive and readily available sources has attained a lot of significance. The present review describes the various recent exploratory works of solar energy H_2 production from H_2S as a more useful alternative to the existing thermal catalytic process, that is, the Claus process used in H_2S processing. © 1997 International Association for Hydrogen Energy

1. INTRODUCTION

Fujishima and Honda [1] in 1971 demonstrated the solarassisted decomposition of water on TiO₂, creating a new chapter in solar energy conversion. H₂S is a VI group hydride like H₂O and can split to give the same amount of H_2 (Fig. 1). H_2S is also a potential source of hydrogen. which is an excellent energy vector. Thus, the photosplitting of H_2S is a more preferable reaction [2] over $H_{2}O$ decomposition. Also the photocleavage of $H_{2}S$ to give H₂ and S has attained a lot of significance as this reaction requires less energy compared to photodecomposition of H₂O. The cleavage of H₂S by two photons requires 9.4 kcal/mol. The high value of H_2 is due to its use as a high quantity energy resource and also its demand as a raw material in the chemical industry. There are difficulties in obtaining H₂ in a pure form at a low cost. In this connection, recovery of H₂ and S from H-S has attracted more attention because of its economic and environmental advantages.

- Economic, since splitting of H₂S in preference of H₂O to produce H₂ is less costly and faster.
- Environmental advantage is the removal of obnoxious smelling H₂S gas which also contributes to acid rain.

Various sources of H₂S are:

- It is an intermediate in several thermochemical cycles.
- Formed as a by-product during the H₂ reduction and

acid bleaching of sulfide as well as from the hydrodesulfurization of petroleum.

• Sour gas streams from geothermal sources often contain a high percentage of $H_2S[3]$ (up to 80% v/v) as in Table 1.

2. PRESENT INDUSTRIAL REMOVAL OF H₂S IS BY CLAUS PROCESS AND WET ABSORPTION PROCESSES

Claus process

It involves partial oxidation of H_2S to S and H_2O where H_2 is wasted. Catalysts like alumina, nickel oxides. etc.. are used in thermal catalytic reactors.

$$H_2S + 3/2O_2 \Rightarrow SO_2 + H_2O$$
$$2H_2S + SO_2 \Rightarrow 3/xS_2 + 2H_2O$$

Fable	1.	H_2S	content,	07 70	by	weight	of	sour	gas	from	selected	
					-10	cations						

Location	H ₂ S			
France (Lacg)	16,0			
West Germany (Varnhorn)	22.4			
Canada (Harmatten, Alberta)	53.5			
Canada (Panther River, Alberta)	7080			
US (Smackover)	22 45			
USSR (Astrakhan)	22.5			
Mainland China	6090			

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Thermochemical cycle for production of hydrogen from H_2O and H_2S . The cleavage of H_2S by two photons requires 9.4 k cal / mol.



$$\Delta G^{\circ} = 2.54 \text{ k cal / photon (1)}$$

$\Delta G^{\circ} = 8.3 \text{ k cal / photon (2)}$



$3H_2S + (3/x)O_2 \Rightarrow (3/x)S_x + 3H_2O$.

The disadvanages of Claus treatment of H₂S are [4]:

- The H₂ component of H₂S is oxidized to H₂O and thus the H₂ is lost.
- Additional tail gas treatment is necessary because the total conversion of the Claus process is not sufficiently high.
- As the refinery acid gases generated from the hydrodesulfurization process are a mixture of hydrocarbons, H₂ and H₂S, separation of these mixed gases (through amine absorption process) is required prior to the Claus process.
- Because of the difficulties in controlling the very high temperature of the gas reaction and maintenance of the catalysts as per the feed gases, the Claus process is considered not to be flexible enough to immediately adjust to changes in the feed.

Wet absorption process

 H_2S is absorbed by Na_2CO_3 or ferric complexed compounds under neutral or weakly alkaline conditions. It is H_2 consuming and available only when the amount or concentration of H_2S is low. Also the rate of regeneration of alkaline or ferric compound by oxidation with air is quite slow.

Other methods for H_2S processing [5]

- Thermochemical methods, direct or indirect splitting of H₂S, using a transition metal sulfide as catalyst (requires a large amount of energy).
- Electrochemical process, using photoelectrochemical cell (apart from solar energy some electrical energy has to be utilized to bring about decomposition of H₂S).
- Photochemical process using photocatalysts and colloidal semiconductor in liquid phases.

Recent investigations by Cervera-March et al. [6] have suggested a photocatalytic method for industrial treatment of H_2S which can be adopted is to mix the outgoing SO₂ and waste gases containing small amounts of H₂S (which feeds the Claus plant) and absorbed in an alkaline aqueous stream. The solar irradiation of the resulting S^{2-}/SO_3^{2-} solutions in the presence of an appropriate photocatalyst yielded H_2 and $S_2O_3^{2-}$. Thiosulfate $(S_2O_3^{2-})$ is also another important by-product of this reaction. They also suggested some schemes of the sulfur route from oil distillates. Linkous et al. [7] have suggested a scheme of a solar photoelectrochemical particle-based process for H₂ and S recovery from H₂S. Several aspects of the proposal system were investigated; first, the need to optimize the activity of the semiconductor particle with catalytic surface atoms is shown, second, consideration of whether to confine the photoparticles to a planar surface within the photoreactor or have them flow over it as a slurry or colloidal suspension is briefly discussed; finally, the chemistry of sulfur and polysulfides is examined to ascertain the best way of generating and collecting clean elemental sulfur from the system.

3. PHOTOCATALYTIC PROCESS

In the photocatalytic process, solar energy which is a renewable energy source, is utilized to bring about photodecomposition of H_2S . Colloidal semiconductors are used as photocatalysts, for example: TiO₂, CdS, CdSe, ZnS, ZnO, CuS, SrTiO₃ [8] etc. Photoinduced charge separation occurs in the semiconductor particles which creates electron/hole pairs. The energy absorbed will be equivalent to its band gap energy. The electron/hole pairs generated move towards the surface of the particle and bring about a redox reaction on the adsorbed substrates.

Semiconductor $\stackrel{hv}{\Rightarrow} e_{CB}^- + h_{VB}^+$.

The holes oxidize S²⁻ in H₂S or HS⁻ to S

$$2\mathbf{h}_{\mathbf{VB}}^{+} + \mathbf{H}_2 \mathbf{S} \Rightarrow 2\mathbf{H}^{+} + \mathbf{S}.$$

The electrons generated reduce H^+ ions present in the medium to H_2 gas.

$$2e_{CB}^{-}+2H^{+} \Rightarrow H_{2}.$$

The overall process corresponds to the cleavage of H_2S by two photons of visible light, which requires 9.4 kcal/mol.

 H_2S + Semiconductor $\stackrel{2hv}{\Rightarrow}$ H_2 + S.

Another possible reaction mechanism is [9]:

 H_2S dissociation: $H_2S + OH^- \Rightarrow HS^- + H_2O$.

Oxidation: $2HS^- + 2h_{VB}^+ \Rightarrow S_2^- + 2H^+$.

Reduction: $2H^+ + 2e_{CB} \Rightarrow H_2$.

Overall: $2H_2S \Rightarrow 2H_2 + 2S$.

Criteria for selecting a photocatalyst are:

- The band gap of the semiconductor should match the solar spectrum facilitating absorption of maximum solar energy from the visible region.
- A good efficiency of solar energy conversion.
- A sufficiently negative flat-band potential to bring about faster hydrogen ion reduction.
- Because of the limited lifetimes of the photogenerated charge carriers even within micron-sized particles, highly crystalline and highly pure semiconductor specimens should be used which give large photocurrents and quantum efficiencies.
- The semiconductor chosen should not be susceptible to photocorrosion, where the photogenerated electron and hole decay by dissolving the surface ions in the electrolyte.

Sacrificial agents

The photocorrosion of the photocatalysts occurs mainly in aqueous solutions and they can be stabilized by reducing agents or sacrificial agents like ferrocyanide, iodide, iron (II)-EDTA complex, sulfide, sulfite, or thiosulfate solutions. Various kinds of sacrificial agents have been tried for the photocatalytic decomposition of H_2S . The sacrificial agents commonly used for this reaction are EDTA [10], sulfide, sulfite or thiosulfate. Sulfide ions are found to be the best sacrificial agents as they can act as hole scavengers.

Depending on the photocatalysts the best sacrificial agent can be chosen, n-type semiconductors like CdS and ZnS are unstable in aqueous solutions, therefore for these semiconductor either an aqueous solution of sulfide ion or a mixture of sulfide and sulfite are ideal. Only sulfite ions instead of sulfide ions give very little yield of H_2 , but a mixture of sulfide and sulfite gives good yield of H_2 . Sulfide is a very good hole scavenger but it influences the reaction indirectly by absorbing sulfur atoms. If the sulfur which is liberated on photodecomposition of H_2S is not removed then it combines with sulfide ion to form colored polysulfide ions which are photon absorbers (400 nm) and thus inhibit the efficiency of the process.

$n\mathbf{S} + \mathbf{S}_2^- \Rightarrow n\mathbf{S}_2^-$ (polysulfides).

Thus removal of sulfur is important and is done by

addition of sulfite ions to sulfur atoms to form thiosulfate ions.

$$S + SO_3^2 \Rightarrow S_2O_3^2$$

Mixed semiconductors

A wide range of photocatalysts are being used in photocatalytic H₂S decomposition. TiO₂ is a good photocatalyst but its bandgap energy lies in the UV region of light and hence it is limited to give high quantum yield. ZnS also has a bandgap energy lying in the UV region of light. CdS/CdSe acts as a good photocatalyst. for this reaction as it has a bandgap energy lying in the visible region of light to efficiently absorb maximum solar energy. A combination of a mixture of two semiconductors, one having lower band gap energy (lying in the visible region) and one having higher bandgap energy (lying in the UV region) can be used very effectively for H₂S decomposition. The electrons and holes produced upon light absorption by this mixture of semiconductors causes the photogenerated electrons to be transferred to the wide bandgap semiconductors and the photogenerated holes into the narrow bandgap semiconductors [11, 12] which gives H_2 evolution and oxidation of sulfide on surfaces of wide and narrow bandgap semiconductors. Furthermore, whenever mixed semiconductors are used, there is intimate contact between the two semiconductors giving rise to an interparticle electron transfer (IPET) which enhances the rate of H₂ production. This intimate contact can also be called a microheterojunction formed between the two semiconductors.

Thiosulfate cycle

It is reported that more efficient solar energy absorption was obtained in mixed semiconductor systems when they are taken in a aqueous mixture of sulfide and sulfite. For instance, CdS loaded with RuO_2 is taken in combination with TiO_2 . Upon irradiation the photogenerated electrons are bringing about reduction of H⁺ and the photogenerated holes react with S²⁻ to form S. This S is absorbed by SO_3^{2-} to give thiosulfate, few photocatalysts like TiO_2 , ZnS or SrTiO₃, except CdS, can further reduce thiosulfate to give back SO_3^{2-} and this forms an efficient thiosulfate cycle where maximum utilization of solar energy is possible [13].

$$CdS \Rightarrow_{(CdS)}e^{-} +_{(CdS)}h^{-}$$

$$_{(CdS)}2h^{+} + S^{2-} \Rightarrow S$$

$$_{(CdS)}2e^{-} + 2H_{2}O \Rightarrow H_{2} + 2OH^{--}$$

$$_{(CdS)}e^{-}TiO_{2} \Rightarrow_{(TiO_{2})}e^{-} + CdS$$

$$_{(TiO_{2})}2e^{-} + 2H_{2}O \Rightarrow H_{2} + 2OH^{--}$$

Loading the TiO₂ particles with a suitable redox catalyst (e.g. RuO₂) leads to more efficient conversion of H₂S to useful products. The energy conversion efficiency is 1%; and in the presence of SO_3^{2-} ions the efficiency is about 2% [14]. By the combination of the two sem-



Fig. 2. Features of a two-compartment system where H₂ is generated.

iconductors, the extent of e^-/h^+ recombination is maximized. Also charge separation is achieved through the selective transfer of e^- from CdS to TiO₂; and thus the transfer of h^+ is thermodynamically inhibited. The working scheme of the two-compartment cell is given in Fig. 2:

$$1.5H_2O + 1.5S_2O_3^{2-} \stackrel{m}{\Rightarrow} 2SO_3^{2-} + S^{2-} + 3H^+.$$

Thus, there are advantages of H_2 production through thiosulfate cycle by decomposition of H_2S .

The advantages of thiosulfate cycle are [13]:

• Light energy is converted to H₂ through a thiosulfate cycle which helps in higher H₂ generation rate. Three moles of H₂ are produced instead of one.

$$3H_2O + S^{2-} \stackrel{hv}{\Rightarrow} SO_3^{2-} + 3H_2$$

• There is neither S nor $S_2O_3^{2-}$ accumulation thus making the photoreaction very efficient.

Use of support materials

The main advantage of semiconductors dispersed on supports over semiconductor bulk powders and dispersions is the very large surface area exposed to reactants and to light. Often because of the high absorption coefficient at the wavelength corresponding to the bandgap, the incident photons are alternated within a short distance from the surface and hence surface properties of catalysts play a dominant role. Various methods are being tried to increase the surface area of the catalysts. The highly dispersed active phase can be achieved by taking the active component on a matrix called a support. Due to its porous microtexture and interfacial interactions the support keeps the active phase in the dispersed state.

Support material in heterogeneous photocatalysis can act as a vehicle for the active phase/component. The large specific surface area of the support maximizes the surface area of the active phase. Typical supports used in the majority of thermal catalysis are Al₂O₃, SiO₂, TiO₂, ZrO₂, Al₂O₃-SiO₂, clay, etc. In the case of mixed semiconductors when both the photocatalysts are supported on one support then the intimate contact between these two semiconductors is increased significantly, bringing about more IPET and thus increasing H_2 production with a good quantum yield.

For example, when ZnS-CdS/Al₂O₃ and ZnS-CdS are tested for photoactivity, the photoactivity of ZnS- CdS/Al_2O_3 was approximately four times higher than ZnS-CdS [15]. The semiconductor on an oxide support may have a bonding interaction between the interface. The semiconductors to be chosen for mixing together must possess matching crystal lattices which facilitate IPET in them. CdS-Cu₂S systems do not give a good yield of H₂ as their crystal lattices do not match and hence the heterojunction between them is not formed, even if they are supported or unsupported [11]. But the metallic Cu deposited on CdS acts as a promoter for CdS photoactivity [16]. CdS-ZnS gives a much higher rate of H₂ evolution since it has very similar crystal lattices facilitating easier transfer of electrons [11]. The energy levels of the conduction band of CdS and ZnS are located at -0.7 and -1.9 eV (NHE), respectively [17]. Since mixtures of CdS and ZnS form homogeneous solid solutions (due to matching crystal lattices), the mixed semiconductor is characterized by a fixed valence band located at +0.7 to +1.9 eV and by a conduction band located between -0.7 and -1.9 eV. By increasing the ZnS fraction, the energy levels of the conduction band of the mixed semiconductors are shifted towards more negative potential values. Compared with pure CdS, this shift is of about -0.2 V for a sample containing 15 mole % ZnS. Therefore, the reduction potential of the conduction band electrons of such a semiconductor would allow more efficient H₂ generation.

The acidic or basic nature of the support may also effect the photoactivity of the catalyst. Recent exploratory work in our laboratory has led to some interesting results. CdS-ZnS systems supported on MgO and y- Al_2O_3 were studied. γ - Al_2O_3 is an acidic oxide and MgO which is a basic oxide were used. The photoactivity of CdS–ZnS/MgO was significantly greater than the photoactivity of CdS-ZnS/yAl₂O₃[18]. Modification of y-Al₂O₃ by base materials like CaO and BaO significantly improved the activity of CdS–ZnS/ γ -Al₂O₃. The basic nature of the support MgO is playing a role in enhancing the activity of CdS-ZnS system. Furthermore, modification of MgO with base materials like Li₂O makes it behave like a super basic oxide and there is a four-fold enhancement in the activity [19] when the same is used as a support for a CdS-ZnS catalyst.

In several instances the catalyst is either coated or deposited on Nafion [20] or polymer films or clays or zeolites or supports [21]. This gives an organized heterogeneous medium which controls the morphology and the photocatalytic activity of the semiconductor. Zeolites are also used as supports for loading semiconductor particles [22]. The zeolite molecules have cage-like structures which can trap the semiconductor particles. Numerous investigations are in progress to explore the best methods

Features of a two-compartment system where H₂ is generated

of H_2S photocatalytic decomposition for obtaining the maximum yields for hydrogen generation.

Use of promoters

Activity in catalysts can also be activated by some promoters like Ag₂S which can motivate CdS and ZnS. Ag₂S acts as a hole scavenger which scavenges the holes by accepting electrons from H₂S [23]. Small amounts of Ag₂S doped on CdS cause activation in the CdS crystal leading to the formation of a microheterojunction. Hole transfer from a CdS particle to S^{2-} ions of the solutions occurs efficiently through CdS/Ag₂S microheterojunctions. The naked CdS exhibits an absorption of 520 nm and the CdS/Ag₂S crystals have an absorption of 620 nm. This effect is attributed to a small part of Ag₂S remaining undissolved. Due to the Ag₂S fraction dissolving in CdS lattice, new silver centres are incorporated into the energetic levels of CdS (bandgap 2.4 eV) and the bandgap shifts to 2.0 eV corresponding to the absorbance of 620 nm [23]. These silver centers are distributed over an energy range of 0.4 eV, just above the valence band of CdS. Radiation with an energy less than the bandgap energy is able to excite electrons from these centers into the conduction band [21]. The same effect is observed when Ag₂S is doped over ZnS and CdS-ZnS mixed semiconductor. Ag₂S doped on CdS-ZnS supported systems also promotes the photoactivity of the system. Metallic silver deposited on CdS also acts as a promoter for CdS photoactivity [19].

4. USE OF METAL DOPANTS

The effective use of electrons and holes obtained by photon absorption of the semiconductor can be achieved only when the charge carriers generated on irradiation can be separated and utilized in the redox reactions within the lifetime of the carrier. Since recombination is one of the predominant routes by which the excitation energy will be dissipated this pathway should be suppressed as far as possible in relation to induced chemical redox reaction. This is achieved in semiconductor photocatalysts by incorporating suitable electron sinks such as deposition of metals like Rh, Pt, Ni, etc. Metal dopants also act as electron transfer agents which help proton reduction. RuO₂ [2] and RuS₂ [24] act as hole transfer agents. The nature of the loaded metal also effects the Ha evolution. The metal to be loaded must be chosen in such a way that it should have high electron affinity and low H_2 over voltage. Pt gives a low H_2 evolution when compared to RuO₂. The presence of metal on the catalysts having low electron affinity and high H₂ over voltage acts as impurity. It also decreases the luminescence intensity of the catalyst. For example a CdO layer decreases the photoactivity of CdS, because the conduction band of CdO is located significantly below that of CdS. Electrons excited in CdS after irradiation can be trapped by the CdO layer [25]. Thus, removal of the CdO layer is necessary. This removal can be done by etching with several agents like acetic acid buffer or diluted HNO₃ or by photocorrosion. RhOx doping on CdS can also help in improving H_2 evolution [26, 27].

Photocatalytic efficiency

Each type of semiconductor such as TiO₂, CdS, ZnS and their mixtures used for photosplitting of H₂S exhibit different efficiencies for producing H₂ depending on the doped promoters and sensitizers. The differences in efficiency may also be due to the bond energy associated with both molecules, the surface states and back reaction between H₂ and S, H₂ and O₂ (dissolved oxygen) [2]. Dissolved O₂ molecules also compete with the proton reduction, thus decreasing the efficiency of the process.

The electrochemical properties of several semiconductor oxides such as WO₃, V₂O₅, ZnO, PbO₂ and CuO are being extensively studied [2] for H₂S photodecomposition. Relatively little is known about the photocatalytic properties of these semiconductors. V₂O₅ and V_2O_4 have been found inefficient for photoproduction of H_2 . There is also ongoing research for H_2 production by colloidal semiconductors like vanadium sulfides and VS loaded with RuO₂. These systems split H₂S at room temperature upon irradiation to give $H_2(g)$ and $Na_2S_2O_3$. A $ZnFe_{2}O_{4}$ [28, 29] system has been found to be active for photocatalytic splitting of H₂S. Also FeS₂ systems have been studied for H₂ evolution but with no success. The methods of preparation, the reaction parameters or conditions and the pre-treatments given to the catalysts during the preparations also effect the semiconductor properties to a greater extent. There are reports where the heat treatment of CdS particles with KCl [30] and KBr [31] changed the surface area of the CdS crystal and enhanced its photoactivity.

Cost analysis

The costs of the catalyst and the reactants H_2S , NaOH. Na₂SO₃ are included in the economic analysis of the process. Here the output cost can be calculated from the energy of H_2 as 68.3 kcal/mol. Furthermore, the hydrogen production cost depends highly on the lifetime of the photocatalyst. Also if the sulphur is recovered more in the thiosulphate compound then it is more attractive. The overall process also needs to minimize the use of non-recyclable chemicals which are used in all the present-day research efforts.

Solar H₂S photolysis plant

A schematic H_2S solar photolysis plant is shown in Fig. 3. After photocatalytic decomposition of H_2S , hydrogen gas is separated. Furthermore, the sulphur or thiosulfate is filtered off. The solution left over is returned to the H_2S absorption tower for further processing.

5. SUMMARY

This article covers methods where H_2S is photodissociated to give the important fuel H_2 . Various



Fig. 3. Schematic diagram of an H₂S solar photocatalytic process.

methods of investigation that are being carried out to bring about maximum production of H_2 using solar energy are discussed. Photodecomposition of H_2S to H_2 and S is a good model reaction which harvests solar energy for production of H_2 and also it is an energy bargain route. Also the chemistry of photodecomposition of H_2S will provide lot of lead points to photodecomposition of H_2O .

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REFERENCES

- 1. Fujishima, A. and Honda, K., Nature, 1992, 37, 238.
- Naman, S. A., Aliwi, S. M. and Al-Emara, K., International Journal of Hydrogen Energy, 1986, 11, 33.
- 3. Kappauf, T., Murray, J. P., Palumbo, R., Diver, R. B. and Fletcher, E. A., *Energy*, 1985, **10**, 1119.
- Isshiki, S., Naguchi, H., Kikuchi, T., Sue, H. and Sakai, K., Industrial and Engineering Chemists Research, 30, 1991.
- Al-Shamma, L. and Naman, S. A., International Journal of Hydrogen Energy, 15, 1990, 1.
- Cervera-March, S. B., Giminks, J., Simano, R. and Andyjar, J. M., International Journal of Hydrogen Energy, 1992, 17, 683.
- 7. Linkous, C. A., Mingo, T. E. and Muradov, N. Z., International Journal of Hydrogen Energy, 1994, 19, 203.
- 8. Matsumura, M., Furukawa, S., Sato, T. and Tsubomura, H., Journal of Physical Chemistry, 1985, 89, 1327.
- 9. Grzyll, C. R., Thomas, J. J. and Barile, R. G., International Journal of Hydrogen Energy, 1989, 14, 647.
- Sabate, J., Cervera-March, S., Simarro, R. and Gimenez, J., International Journal of Hydrogen Energy, 1990, 15, 115.
- 11. Savinov, E. N., Gruzdkov, A. Yu. and Parmon, Y. N., International Journal of Hydrogen Energy, 1989, 14, 1.

- 12. Serpone, N., Borgarello, E. and Gratzel, M., Journal of the Chemical Society, Chemical Communications, 384, 1984.
- Borgarello, E., Desilvesto, J., Gratzel, M. and Pelizett, E., Separatum Helvetica Chimico Acta, 1983, 66, 1827.
- Serpone, N., Lavolen, D., Terzian, R., Minero, C. and Pelizetti, E., *Photochemical Conversion and Storage of Solar Energy*, 451, 1991.
- Kabayashi, J., Kitaguchu, K., Tsuiki, H., Ueno, A. and Kotera, Y., Chemical Letters, 1985, 627.
- Gruzdkov, Yu. A., Savinov, E. N. and Parmon, V. N., International Journal of Hydrogen Energy, 1987, 12, 393.
- 17. Reber, J. F. and Rusek, M., Journal of Physical Chemistry, 1986, 90, 824.
- Subrahmanyam, M., Supriya, V.T. and Ram Reddy, P., International Journal of Hydrogen Energy, 1995, 21, 99.
- Supriya, V. T. and Subrahmanyam, M., Proceedings of Eleventh International Conference on Photochemical Conversion and Storage of Solar Energy (IPS-II), Bangalore. August 1996.
- Sato, T., Maseki, K., Yashioka, T. and Okurwaki, A., Journal of Chemical and Technical Biotechnology, 1993, 58, 315.
- Makhmadurodov, A., Gnuzdkov, Yu. A., Saninov, E. N. and Parmon, V. N., translated from *Kinetika kataliz*, 27, 1986.
- Liu, X., Lu, K. and Thomas, K. J., Journal of the Chemical Society, Faraday Transactions, 1993, 89, 1861.
- Taqui Khan, M. M., Bharadwaj, R. C. and Bharadwaj, C., International Journal of Hydrogen Energy, 1988, 13, 7.
- Harry, D., Thewisson, M. W., Vander Zouwen, E. A., Timmer, A. K., Alois, H. A, Tinnemanns and Mack, A., Journal of the Chemical Society, Chemical Communications, 941, 1984.
- Buhler, N., Meier, K. and Reber, J. F., Journal of Physical Chemistry, 1984, 88, 3261.
- Kosanic, M. M. and Topalov, A. S., International Journal of Hydrogen Energy, 1990, 15, 319.

- 27. Topalov, A. S., Jovanovic, L. S. and Serb, M. J., Chemical Society, 56(II), 1991.
- Lu, G. and Li, S., International Journal of Hydrogen Energy, 1992, 17, 767.
- 29. Li, S. and Lu, G., New Journal of Chemistry, 1992, 16.
- Kobayakawa, K., Miura, T., Suzuki, A., Sato, Y. and Fujishima, A., Solar Energy Materials and Solar Cells, 1993, 30, 201.
- Kobayakawa, K., Inque, T., Sato, Y. and Fujishima, A., Denki Kagaku, 1993, 61, 874.
- 32. Borgarello, E., Serpone, N., Gretzel, M. and Pellizetti, E., International Journal of Hydrogen Energy, 1985, 10, 737.
- Rajh, T. and Micic, O. I., Bulletin Dela Societe E. Chinique Beograd, 1983, 48, 335.
- 34. Subrahmanyam, M., Wireless photocatalysis. Proceedings of 3rd International Symposium on Advances in Electrochemical Science and Technology, Madras, December 1984.
- Barbeni, M., Pelizzetti, E., Borgarello, E., Serpone, N., Gratzel, M., Balducci, L. and Visca, M., *International Jour*nal of Hydrogen Energy, 1985, 10, 249.
- 36. Andelka, S., Ljiljana, T., Jovanovic, S., Kosanic, M. and lav, *Journal of Serb-Chemical Society*, 1991, **56**, 637.
- Borgarello, E., Serpone, N., Pellizzetti, E. and Barbeni, M., Journal of Photochemistry, 1986, 33, 35.
- 38. Subrahmanyam, M., Energy Management, 1985, 9, 25.
- 39. Naman, S. A. and Emara, Al., International Journal of Hydrogen Energy, 1987, 12, 629.
- Borgarello, E., Terzian, R., Serpone, N., Pelizzetti, E. and Barbeni, M., Inorganic Chemistry, 1986, 25, 4499.

- 41. Zeltner, W. A., Hiv, C. G., Mar, A. Jr. and Anderson, *Chem* Tech., 21, May 1993.
- Subrahmanyam, M., Renuka, B. R. and Vinaykumar, M., Advances in Hydrogen Energy, 1986, 5 (Hydrogen Energy Prog. 6,3) 1403, Pergamon Press, New York, 1987.
- 43. Fox, M. A., Chemtech., 680, Nov. 1992.
- Sundaram, K. K., Borgarello, E. and Gratzel, M., Helvetica Chemica Acta, 1981, 64, 35.
- Pelizzetti, E., Borgarello, E., Serpone, N. and Gratzel, N. M., *Catalysis on the Energy Scene*. Elsevier Science Publishers, Amsterdam, 1984, p. 327.
- Borrell, L., Cervera-March, S., Gimenez, J. and Simano, R., Solar Energy Materials and Solar Cells, 1992, 25, 25.
- Subrahmanyam, M., Particulate and Multiphase Processes. ed. T. Airman and T. N. Veziroglu. 3. 391. Hemisphere Publishing Corporation, USA, 1987.
- Naman, S. A., International Journal of Hydrogen Energy, 1992, 17, 499;
- Megalofonos, S. K. and Papayannakos, N. G., International Journal of Hydrogen Energy, 1991, 16, 319.
- Rufus, I. B., Vishwanathan, B., Ramakrishnan, V. and Kuriacose, J. C., Journal of Photochemistry and Photobiology, A. Chemistry, 1995, 91, 63.
- Subrahmanyam, M., Alternative Energy Sources, VII, ed. T. N. Veziroglu. Hemisphere Publishing Corporation, USA, 1987, pp. 225–235.
- Subramanyam, M., Present status of catalysis in solar energy conversion. Sixth national workshop cum seminar on Catalysis in Energy Conversion and Environment. Dhanbad, 1991.