

# An XPS study of dispersion and chemical state of MoO<sub>3</sub> on Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> binary oxide support

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## Abstract

X-ray photoelectron spectroscopy (XPS) technique was employed to characterize Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> support and MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> catalyst calcined at different temperatures from 773 to 1073 K. The Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> (1:1.3 mole ratio) binary oxide support was obtained by a coprecipitation procedure with in situ generated ammonium hydroxide. A nominal 12 wt.% MoO<sub>3</sub> was impregnated over the calcined (773 K) support by a wet impregnation method. The initial characterization by X-ray powder diffraction, Fourier transform-infrared (FT-IR), and O<sub>2</sub> chemisorption techniques revealed that the impregnated MoO<sub>3</sub> is in a highly-dispersed state on the surface of the support. XPS electron binding energy ( $E_b$ ) values indicate that the MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> catalyst contains the mixed-oxide elements in the highest oxidation states, Ti(IV), Al(III), and Mo(VI), respectively. However, the core level  $E_b$  of Al 2p slightly increased with increase of calcination temperature, and this effect was more prominent in the case of molybdena-doped samples. A better resolved Mo 3d doublet was observed at all calcination temperatures. This was explained as due the coverage of alumina surface by titania, thereby lowering the interaction between molybdena and alumina. The XPS atomic ratios indicate that the Ti/Al ratio is sensitive to the calcination temperature. The Mo/Al ratio was found to be more than that of Mo/Ti ratio and decreased with increasing calcination temperature. A clear difference between the Al<sub>2</sub>O<sub>3</sub> and the TiO<sub>2</sub> surfaces, in terms of surface free energy, isoelectric point, and surface hydroxyl distribution was considered to be responsible for different distributions of molybdena over these supports. © 2001 Elsevier Science B.V. All rights reserved.

*Keywords:* Molybdena; Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub>; MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub>; Mixed oxide; XPS; XRD; Dispersion; Thermal stability

## 1. Introduction

Supported-molybdenum oxide catalysts are widely used in various catalytic processes. The molecular structure of molybdenum oxide on different supports has also been extensively investigated by var-

ious techniques over the past decade [1,2]. Several studies in the literature employing Raman, Fourier transform-infrared (FT-IR), solid state <sup>95</sup>Mo nuclear magnetic resonance (NMR), extended X-ray absorption fine structure (EXAFS), X-ray absorption near edge structure (XANES), X-ray photoelectron spectroscopy (XPS), and ultraviolet visible diffuse reflectance spectroscopies (UV-DRS) have concluded that the surface structure of supported-molybdenum

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oxide is highly sensitive to the nature of support, molybdenum oxide loading, extent of surface hydration and dehydration, surface impurities, and calcination temperature [3–16]. In particular, the structure of molybdenum oxide/sulfide on alumina support has been extensively studied under ambient, dehydrated, and reaction conditions [2,11, 14–16].

Besides alumina, there has been an increasing amount of interest over the past few years on other supports, such as titania, zirconia, ceria, and activated carbon. Molybdena-titania combination is an excellent catalyst or catalyst precursor for gas–oil hydrotreatment [17], alkene metathesis [18], and selective oxidation of hydrocarbons [19]. For example, the intrinsic activity of Mo atom on  $\text{TiO}_2$  was 1.5 times more than that on the  $\text{Al}_2\text{O}_3$  support for hydrogenation of a model reaction, tetralin [20]. However, a major disadvantage associated with  $\text{TiO}_2$  support is its low specific surface area and low thermal stability of the active anatase structure at high temperatures. To overcome these deficiencies, titania was combined with alumina or silica, by taking advantage of the high thermal stability of  $\text{Al}_2\text{O}_3$  or  $\text{SiO}_2$  to stabilize the specific surface area and the structure of anatase. A few studies concerning the structural and catalytic properties of  $\text{TiO}_2$ - $\text{Al}_2\text{O}_3$  mixed oxides have been reported [20–26]. For example, the  $\text{MoO}_3$  when supported on  $\text{TiO}_2$ - $\text{Al}_2\text{O}_3$  was found to exhibit better catalytic performance for hydrodesulfurization reaction [22].

The primary objective of this study was to follow the structure evaluation of  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  mixed oxide support and the dispersion and nature of molybdenum oxide phase on this support under the influence of thermal treatments. X-ray photoelectron spectroscopy (XPS or ESCA), because of its high surface sensitivity (probing depth ca. 2 nm), has been considered as one of the best techniques for studying the dispersion of transition metal oxides on various supports and to gain knowledge on the type of interaction involved between the active metal oxide species and the supporting oxide [27–30]. In the present investigation, the XPS technique was applied to get more information on the preferential interaction of molybdenum oxide with alumina and/or titania components of the binary oxide support.

## 2. Experimental

### 2.1. Catalyst preparation

The  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  (1:1.3 mole ratio) support was prepared by a homogeneous coprecipitation method with in situ generated ammonium hydroxide by decomposition of urea at 368 K. To achieve this, a mixed aqueous solution of  $\text{NaAlO}_2$  (Loba Chemie, GR grade),  $\text{TiCl}_4$  (Fluka, AR grade), and urea (Loba Chemie, GR grade) was heated to 368 K with vigorous stirring. In about 6 h of heating, as decomposition of urea progressed to a certain extent, the formation of precipitate gradually occurred. The precipitate was heated for 6 h more to facilitate aging. Thus, formed coprecipitate was filtered-off, washed several times with deionized water until free from chloride ions, and dried at 393 K for 16 h. To remove residual sodium ions, the oven-dried precipitates were again washed with ammonium nitrate solution (5%) several times, followed by hot distilled water, and dried once again at 383 K for 12 h. The obtained sample was finally calcined at 773 K for 6 h in open-air atmosphere. Some portions of this finished  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  support were once again heated at 873, 973, and 1073 K for 6 h in a closed electrical furnace in open-air atmosphere.

To make  $\text{MoO}_3$ / $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  catalyst, a nominal 12 wt.%  $\text{MoO}_3$  was deposited on the  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  support by a standard wet impregnation method. To impregnate  $\text{MoO}_3$ , the requisite quantity of ammonium heptamolybdate (JT Baker, UK, AR grade) was dissolved in doubly-distilled water, and the finely-powdered calcined (773 K) mixed oxide support was added to this solution. The excess water was evaporated on a water bath with continuous stirring. The resultant solid was then dried at 383 K for 12 h and calcined at 773 K for 6 h in a closed electrical furnace in open-air atmosphere. Some portions of the finished catalyst were once again heated at 873, 973, and 1073 K for 6 h in a closed electrical furnace in open-air atmosphere. The rate of heating (as well as cooling) was always maintained at  $10 \text{ K min}^{-1}$ .

### 2.2. Catalyst characterization

X-ray powder diffraction patterns have been recorded on a Siemens D-5000 diffractometer by using  $\text{Cu K}\alpha$  radiation source. The XRD phases present in

the samples were identified with the help of JCPDS files. The X-ray line broadening technique was used to determine the crystallite size of TiO<sub>2</sub> anatase in the samples from XRD data of (1 0 1) reflection. The FT-IR spectra were recorded on a Nicolet 740 FT-IR spectrometer at ambient conditions using KBr discs with a nominal resolution of 4 cm<sup>-1</sup> and averaging 100 spectra. Oxygen chemisorption measurements were made as per the procedure described elsewhere [31].

The XPS measurements were made on a VG Scientific ESCA Lab 210 spectrometer. The Mg K $\alpha$  and Al K $\alpha$  radiations were used as excitation sources. The spectra were recorded in the fixed analyzer transmission mode, the pass energy being 50 eV. The scanning of the spectra was done at pressures less 10<sup>-8</sup> Torr. The Ti 2p<sub>3/2</sub> or C 1s lines were taken as internal references with a binding energy of 458.5 and 285.0 eV, respectively [32]. An estimated error of  $\pm 0.1$  eV can be assumed for all the measurements. Quantitative analysis of atomic ratios was accomplished by determining the elemental peak areas, following a Shirley background subtraction by the usual procedures [32–34], and carried out using the sensitivity factors supplied with the instrument. The modified Auger parameter of Ti and Al was calculated according to the following equations:

$$\alpha^I(\text{Ti}) = \alpha + h\nu = \text{BE of the Ti } 2p_{3/2} \text{ peak} \\ + \text{KE of the Ti } L_3M_{23}V \text{ Auger peak}$$

$$\alpha^I(\text{Al}) = \alpha + h\nu = \text{BE of the Al } 2p \text{ peak} \\ + \text{KE of the Al } KL_{23}L_{23} \text{ Auger peak}$$

where BE is the binding energy and KE the kinetic energy [35,36].

### 3. Results and discussion

The alumina-titania binary oxide support calcined at 773 K exhibited a specific surface area of 159 m<sup>2</sup> g<sup>-1</sup>. Therefore, a 12 wt.% MoO<sub>3</sub> was selected to impregnate over the support surface to achieve a monolayer coverage [37,38]. The X-ray powder diffraction analysis of MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> catalyst (773 K) also revealed that there are no XRD lines due to crystalline MoO<sub>3</sub>, except the broad diffraction lines due to TiO<sub>2</sub>

anatase. The FT-IR spectra of the sample also supported the XRD observations. The O<sub>2</sub> chemisorption measurements obtained as per the procedure described elsewhere [31] also revealed that the MoO<sub>3</sub> is in a highly-dispersed state on the support surface at 773 K calcination temperature. Chemisorption of O<sub>2</sub> is possible only on the reduced Mo oxide, which contains coordinately-unsaturated sites. The O<sub>2</sub> chemisorption method discriminates between the monolayer and crystalline Mo oxide phases, since their reduction behaviors are entirely different [39]. The preliminary characterization results thus suggest that the impregnated molybdena is in a highly-dispersed state on the surface of the Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> support. In other words, there is no excess MoO<sub>3</sub> in the microcrystalline form on the Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> carrier when calcined at 773 K.

To understand the temperature stability of the Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> support and the MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> catalyst, samples were subjected to high temperature treatments from 773 to 1073 K. The BET surface area of the Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> support was found to decrease from 159 m<sup>2</sup> g<sup>-1</sup> at 773 K to 32 m<sup>2</sup> g<sup>-1</sup> at 1073 K due to sintering. The sintering effect was little larger in the case of molybdena-impregnated samples. The BET surface area of the 12% MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> catalyst was observed to decrease from 96 m<sup>2</sup> g<sup>-1</sup> at 773 K to 26 m<sup>2</sup> g<sup>-1</sup> at 1073 K. The XRD patterns of Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> exhibited only anatase phase, and the intensity of the lines due to this phase was observed to increase with increasing calcination temperature. The crystallite size of anatase increased from ca. <3.5 nm at 773 K to 15.1 nm at 1073 K. There is no evidence in the literature about the existence of solid solutions between alumina and titania. However, the formation of only one definite compound Al<sub>2</sub>TiO<sub>5</sub> was reported above 1273 K temperature [40]. The dispersed MoO<sub>3</sub>, in the case of MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> catalysts, was found to exhibit some influence on the crystallization of anatase. The crystallite size of anatase increased from 5.1 nm at 773 K to 18.6 nm at 1073 K. Some broad diffraction lines due to Al<sub>2</sub>(MoO<sub>4</sub>)<sub>3</sub> compound together with TiO<sub>2</sub> rutile lines were noted at 1073 K.

The samples of Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> and MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> calcined at different temperatures have been investigated by XPS technique. The photoelectron peaks of O 1s, Ti 2p, Al 2p, and Mo 3d are presented in Figs. 1, 2, 3 and 4, respectively. For the purpose of better comparison, the XPS photoelectron peaks of

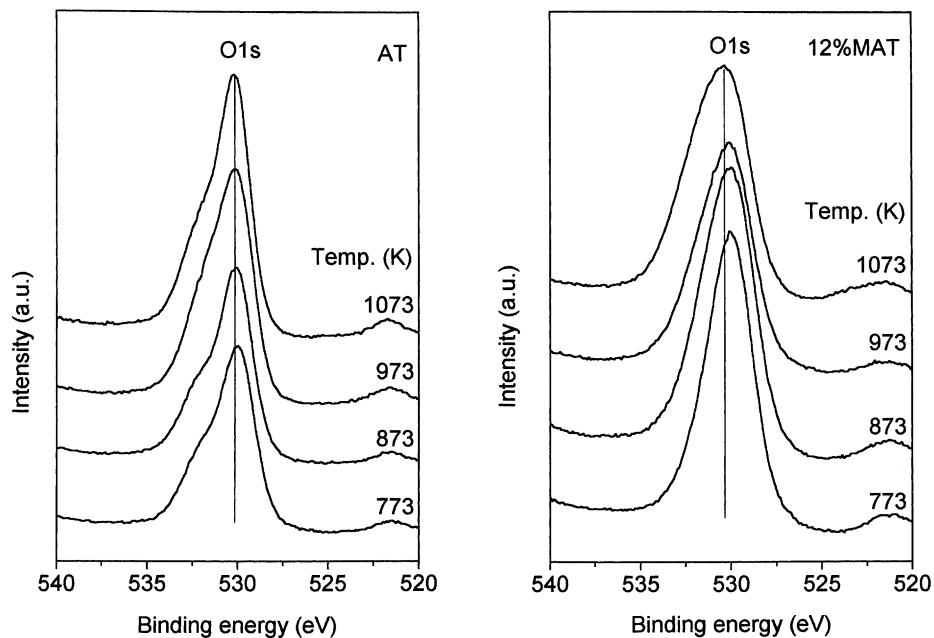


Fig. 1. XPS of the O 1s binding energy region for Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> (AT) support and MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> (12% MAT) catalyst calcined at different temperatures.

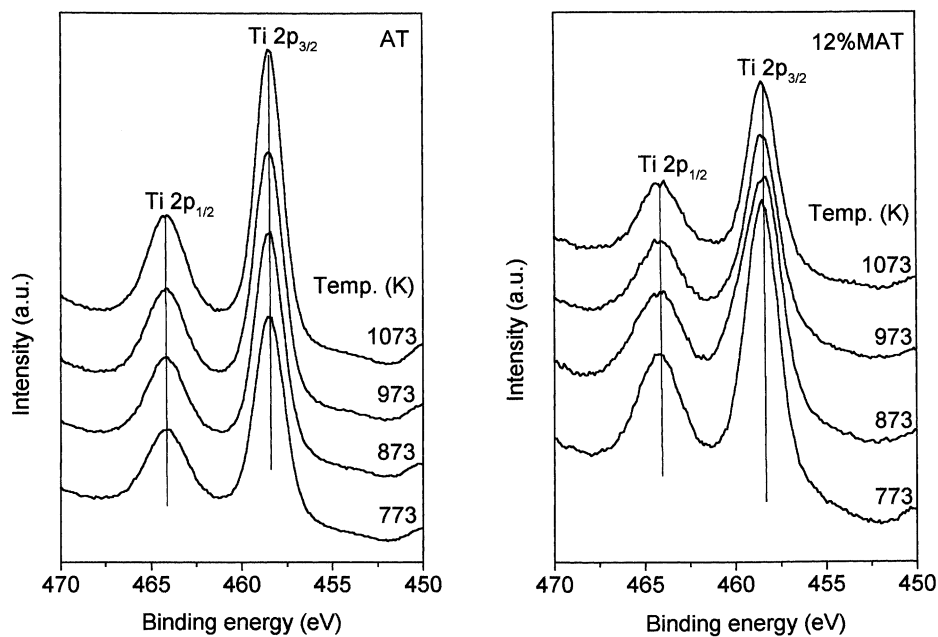


Fig. 2. Ti 2p XPS spectra of Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> (AT) support and MoO<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> (12% MAT) catalyst calcined at different temperatures.

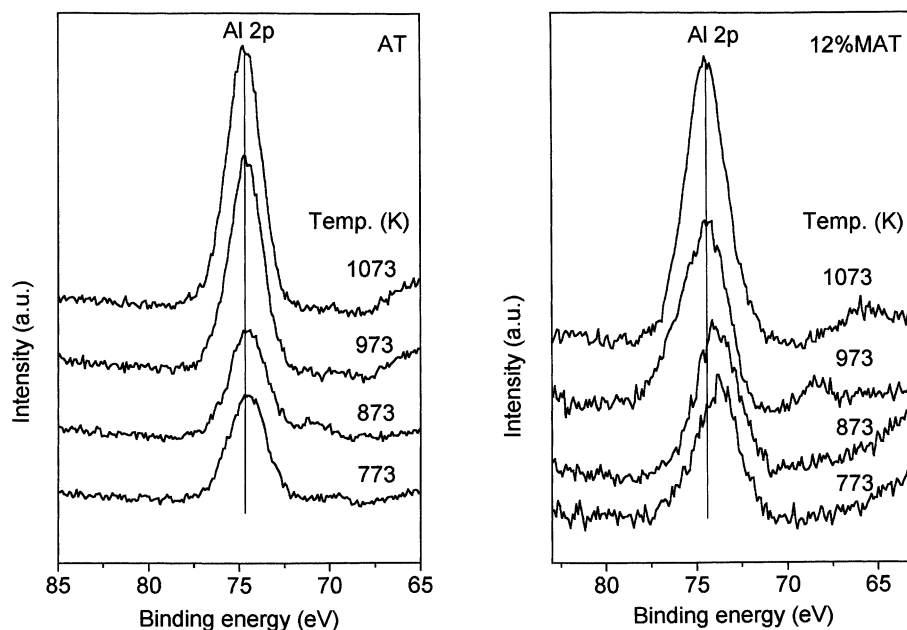


Fig. 3. Al 2p XPS spectra of  $\text{Al}_2\text{O}_3\text{-TiO}_2$  (AT) support and  $\text{MoO}_3/\text{Al}_2\text{O}_3\text{-TiO}_2$  (12% MAT) catalyst calcined at different temperatures.

O 1s, Ti 2p, and Al 2p pertaining to the  $\text{Al}_2\text{O}_3\text{-TiO}_2$  binary oxide support and the corresponding peaks of the  $\text{MoO}_3/\text{Al}_2\text{O}_3\text{-TiO}_2$  catalyst are shown together in these figures. The corresponding electron binding

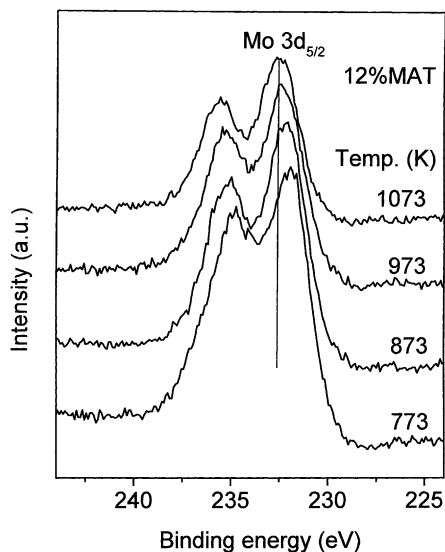


Fig. 4. Mo 3d XPS spectra of  $\text{MoO}_3/\text{Al}_2\text{O}_3\text{-TiO}_2$  (12% MAT) catalyst calcined at different temperatures.

energies ( $E_b$ ) and the Auger parameter values are presented in Table 1. In general, the intensity of all photoelectron peaks increased with increasing calcination temperature. This general effect is also accompanied by a diminution of C 1s peak intensity, which indicates clearly that the calcination treatment is also cleaning the surface of the samples from carbon contamination. The O 1s profile (Fig. 1) is, in general, complicated due to the overlapping contribution of oxygen from titania and alumina in the case of the  $\text{Al}_2\text{O}_3\text{-TiO}_2$  support and from titania, alumina, and molybdena in the case of the  $\text{MoO}_3/\text{Al}_2\text{O}_3\text{-TiO}_2$  catalyst. Two oxygen peaks are observed for the  $\text{Al}_2\text{O}_3\text{-TiO}_2$  support at all calcination temperatures. The O 1s line with  $E_b = 530.0\text{--}530.4\text{ eV}$  can be assigned to the lattice oxygen of the  $\text{TiO}_2$ . The second O 1s line at higher binding energy ( $E_b = 531.1\text{--}531.4\text{ eV}$ ) is due to  $\text{Al}_2\text{O}_3$ . This assignment is easily possible judging from the difference in the electronegativity of the elements involved [41] and also from the literature [42]. Overlapping contribution from molybdena made it difficult to discriminate the different oxygen peaks in the case of the  $\text{MoO}_3/\text{Al}_2\text{O}_3\text{-TiO}_2$  catalyst. The pure  $\text{MoO}_3$  exhibits a sharp O 1s peak at  $E_b = 530.62$  [43]. In the case of the  $\text{Al}_2\text{O}_3\text{-TiO}_2$  carrier, the

Table 1

Electron binding energies ( $E_b$ ), modified Auger parameter values, and XPS atomic ratios for  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  support and 12 wt.%  $\text{MoO}_3/\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  catalyst calcined at different temperatures<sup>a</sup>

| Temperature (K)   | Ti 2p <sub>3/2</sub> | Ti KE | $\alpha^I$ (Ti) | Al 2p | Al KE  | $\alpha^I$ (Al) | O 1s  | Mo 3d <sub>5/2</sub> | Ti/Al | Mo/Ti | Mo/Al |
|---|----------------------|-------|-----------------|-------|--------|-----------------|-------|----------------------|-------|-------|-------|
| <b><math>\text{Al}_2\text{O}_3</math>-<math>\text{TiO}_2</math> support</b>               |                      |       |                 |       |        |                 |       |                      |       |       |       |
| 773   | 458.5                | 414.6 | 873.1           | 74.5  | 1387.5 | 1462.0          | 530.0 |                      | 2.58  |       |       |
| 873   | 458.5                | 414.7 | 873.2           | 74.6  | 1387.4 | 1462.0          | 530.1 |                      | 2.02  |       |       |
| 973   | 458.5                | 414.6 | 873.1           | 74.6  | 1387.2 | 1461.8          | 530.1 |                      | 1.57  |       |       |
| 1073  | 458.5                | 414.7 | 873.2           | 74.7  | 1387.0 | 1461.7          | 530.2 |                      | 1.20  |       |       |
| <b><math>\text{MoO}_3/\text{Al}_2\text{O}_3</math>-<math>\text{TiO}_2</math> catalyst</b> |                      |       |                 |       |        |                 |       |                      |       |       |       |
| 773   | 458.5                | 415.0 | 873.5           | 74.2  | 1388.2 | 1462.4          | 530.0 | 232.1                | 1.67  | 0.31  | 0.37  |
| 873   | 458.5                | 415.1 | 873.6           | 74.5  | 1387.7 | 1462.2          | 530.3 | 232.3                | 1.16  | 0.30  | 0.35  |
| 973   | 458.5                | 415.3 | 873.8           | 74.6  | 1387.3 | 1461.9          | 530.6 | 232.6                | 1.00  | 0.28  | 0.33  |
| 1073  | 458.5                | 415.4 | 873.9           | 74.8  | 1386.7 | 1461.5          | 530.7 | 232.7                | 0.48  | 0.25  | 0.18  |

<sup>a</sup> All values are in electron volts, eV, except atomic ratios.

binding energy of the most intense O 1s peak (Table 1) is almost constant with increase of calcination temperature. However, a clear increase in the binding energy of the O 1s peak with temperature is observed for molybdena-doped samples. This may be due to the segregation of molybdenum oxide on the support surface or the formation of  $\text{Al}_2(\text{MoO}_4)_3$  compound with increase of calcination temperature [15].

Fig. 2 shows the Ti 2p photoelectron peaks at  $E_b = 458.5$  and  $464.4$  eV for Ti 2p<sub>3/2</sub> and Ti 2p<sub>1/2</sub> lines, respectively, which agree well with values reported in the literature [41,44,45]. It is interesting to note that the intensity of the Ti 2p core level spectra, in the case of  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  mixed oxide, increased with increasing calcination temperature. This may be due to two reasons: the first one is the elimination of residual carbon during calcination of the samples in air at higher temperatures, and the other one is the crystallization of titania with increase of calcination temperature as observed from XRD studies. The Auger parameter for Ti has also been measured and summarized in Table 1. A small but insignificant variation can be seen for all the samples. As this parameter does not depend on charge effects, Ti seems to be in a similar chemical state in all the samples. Therefore, Ti was considered as a good reference for binding energy calibrations [36,45,46]. The results thus suggest that the titania in the  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  support and in the  $\text{MoO}_3/\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  catalyst is in the highest oxidation state of Ti(IV) irrespective of high temperature treatments.

Fig. 3 shows the Al 2p photoelectron peak of the samples calcined at various temperatures. The corre-

sponding binding energies and the Auger parameter values are shown in Table 1. An insignificant slight increase in the core level  $E_b$  and decrease in the Auger parameter value can be noted with increasing calcination temperature. These changes in the binding energy ( $E_b = 74.2$ – $74.8$  eV) and the Auger parameter value ( $\alpha^I = 1462.4$ – $1461.5$  eV) are slightly larger in the case of  $\text{MoO}_3/\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  catalyst, in comparison to the pure support ( $E_b = 74.5$ – $74.7$  eV and  $\alpha^I = 1462.0$ – $1461.7$  eV). The slight increase in binding energy and decrease in Auger parameter values may be explained to be due to the disappearance of the surface hydroxyl groups of the alumina support. On thermal treatment, water is normally evolved from two neighboring hydroxyl ions which leave the coordination sphere of an aluminum ion incomplete. So, there is a removal of negative charge density from the alumina center due to dehydroxylation, which has been reflected in the binding energy. Dehydroxylation is more in the case of molybdena-doped samples due to formation of Mo–O–Al bonds during calcination by exchange of surface hydroxyl groups between the active component and the support [14,15,47]. As per the literature, there is also a small increase in the  $E_b$  of Al 2p during transformation of  $\text{Al}_2\text{O}_3$  from  $\gamma$ - to the  $\alpha$ -phase under the influence of thermal treatments beyond 873 K [48]. However, the XRD technique failed to detect the lines due to  $\alpha$ - $\text{Al}_2\text{O}_3$  phase in the samples calcined up to 1073 K due to poor crystallinity of this phase. However, its presence was noted at 1273 K calcination. An increase in the  $E_b$  of Al 2p was also noted due to the formation of  $\text{Al}_2(\text{MoO}_4)_3$  between

$\text{Al}_2\text{O}_3$  and  $\text{MoO}_3$  oxides [49]. These observations reveal that the alumina in the mixed oxide may probably convert partially from the metastable gamma to the stable alpha phase in the case of pure support, and to a definite  $\text{Al}_2(\text{MoO}_4)_3$  compound in the case of  $\text{MoO}_3/\text{Al}_2\text{O}_3\text{-TiO}_2$  catalyst at higher calcination temperatures. As reported in the literature, the Auger parameter is known to provide information about the electronic properties of the oxides dispersed on metal or metal oxides [35,46]. The binding energy and the Auger parameter of  $\text{TiO}_2$  deposited on  $\text{SiO}_2$  have been changed by 0.7 and 2.6 eV as the coverage increases [36]. The observed small variation in the binding energy and the Auger parameter value of aluminum in comparison to titanium indicate that the former might have been modified due to the influence of the  $\text{TiO}_2$  support. To establish this fact, further studies are essential with different loadings of alumina on titania. However, it is not the primary goal of this investigation. As can be seen from Fig. 3, a sharp rise in the intensity of the Al 2p core level peak with increase in calcination temperature has been observed for both cases. Surface enrichment of alumina particles may be one of the causes for this observation, which will be dealt in the latter paragraphs. In summary, it is evident from Fig. 3 that the Al 2p photoelectron peak depends on the calcination temperature as well as on the coverage by molybdenum oxide on the alumina-titania carrier.

The XPS Mo 3d<sub>5/2</sub> photoelectron peak of  $\text{MoO}_3/\text{Al}_2\text{O}_3\text{-TiO}_2$  sample calcined at various temperatures is shown in Fig. 4. As can be noted from this figure, the Mo 3d doublet is well resolved at all temperatures. However, the intensity has been decreased with increase of calcination temperature from 773 to 1073 K. There is a slight increase in the  $E_b$  (232.1–232.7 eV) of Mo 3d with increase of calcination temperature. The core level binding energy values indicate that the molybdenum is present in Mo(VI) state and coincides with the literature [28,50]. The slight increase in the  $E_b$  with increase of calcination temperature further provides an impression that the dispersed molybdenum may be present in the octahedral Mo(VI) state at lower temperatures and tetrahedral Mo(VI) state due to the formation of  $\text{Al}_2(\text{MoO}_4)_3$  ( $E_b = 232.7$  eV) at higher calcination temperatures [28,49]. It has been reported earlier that a strong interaction between molybdena and alumina

favors the presence of more than one type of Mo(VI) species on the alumina surface. Therefore, the XPS Mo 3d doublet was quite broad for  $\text{MoO}_3/\text{Al}_2\text{O}_3$  catalyst [28]. However, Mo species has more uniform geometrical and chemical characteristics on titania surface, which makes the Mo 3d peaks well resolved in the case of  $\text{MoO}_3/\text{TiO}_2$  catalyst [28]. The structure of surface molybdenum oxide species are primarily isolated, tetrahedrally coordinated at lower loadings, and tend towards polymerized, octahedrally coordinated at higher loadings (near or above monolayer coverage) [14,15,28]. At monolayer coverage, the structure of surface molybdenum oxide species primarily possesses an octahedral coordination on  $\text{TiO}_2$  and a mixture of tetrahedral and octahedral coordination on  $\text{Al}_2\text{O}_3$ . As mentioned earlier, in the present investigation a well-resolved Mo 3d doublet peak is observed like the one reported for  $\text{MoO}_3/\text{TiO}_2$  catalysts. A partial coverage of alumina surface with titania ( $\text{Al}_2\text{O}_3:\text{TiO}_2 = 1:1.3$  mole ratio) lowers the interaction between molybdena and alumina, thereby better resolving the Mo 3d doublet peak similar to those of pure titania-supported catalysts. The XPS atomic ratios described in the next paragraph also support these observations.

The Mo/Al, Mo/Ti, and Ti/Al atomic ratios, as determined by XPS, for the 12 wt.%  $\text{MoO}_3/\text{Al}_2\text{O}_3\text{-TiO}_2$  catalyst and for the  $\text{Al}_2\text{O}_3\text{-TiO}_2$  support, respectively, are calculated and shown in Fig. 5 and Table 1. As can be noted from Table 1 and Fig. 5b, the Ti/Al atomic ratio is slightly more for pure support than that of molybdena-doped samples at all calcination temperatures. This observation indicates that molybdenum oxide over-layer has covered the  $\text{Al}_2\text{O}_3\text{-TiO}_2$  support surface. Further, the Ti/Al atomic ratio has been decreased with increase of calcination temperature for both cases. For the pure support, taking into account the fact that the surface free energies of  $\text{TiO}_2$  (0.280–0.380  $\text{N m}^{-1}$ ) are less than those of  $\text{Al}_2\text{O}_3$  (0.650–0.925  $\text{N m}^{-1}$ ); the dispersion of titania on alumina is favored according to the thermodynamic rule [51]. The initial surface enrichment of  $\text{TiO}_2$  at lower temperatures makes the Ti/Al intensity ratio greater. There could be another explanation also that during precipitation process, microparticles containing titanium previously deposited can act as nucleation centers and cause  $\text{TiO}_2$  coverage on  $\text{Al}_2\text{O}_3$  to take the form of a tower structure [52]. With increase of

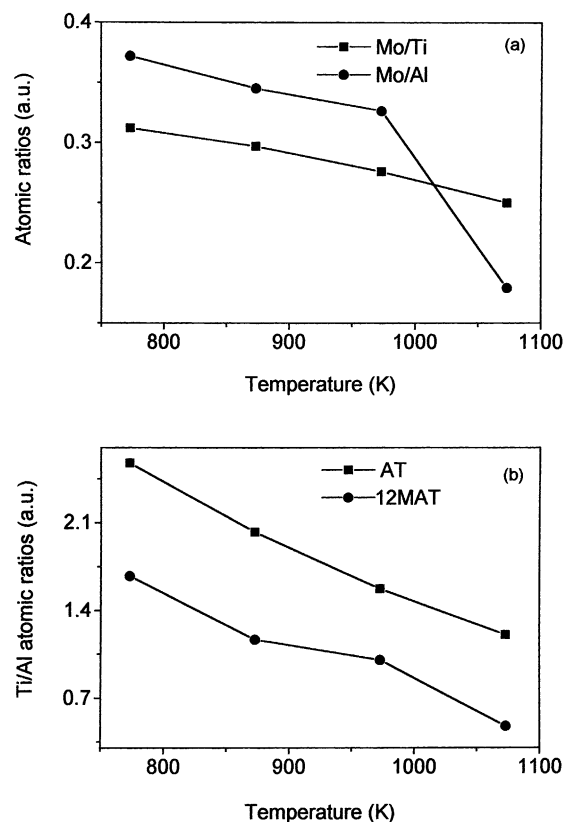


Fig. 5. XPS atomic ratio vs. calcination temperature for the  $\text{Al}_2\text{O}_3\text{-TiO}_2$  (AT) support and  $\text{MoO}_3/\text{Al}_2\text{O}_3\text{-TiO}_2$  (12% MAT) catalyst calcined at different temperatures.

calcination temperature, surface enrichment of aluminum particles may occur due to thermally-induced mobility of those particles driven by concentration gradient. In coprecipitation, incorporation of one ion into another oxide matrix is a well-known fact. The ionic radius of octahedrally-coordinated Ti(VI) is  $0.605 \text{ \AA}$  in contrast to the radius of octahedrally-coordinated Al(III) ions which is  $0.53 \text{ \AA}$  [53]. A relatively slight difference between the sizes of these cations suggests that Ti can substitute partially Al in the octahedral sites of alumina during the preparation method. Due to different charges of Ti and Al cations, this substitution requires that close cationic sites should remain partially vacant. For every three Ti cations substituting for Al, one site can remain vacant. The increase in lattice vacancies helps the diffusion of smaller aluminum ions more towards the surface by heat treatment.

As can be seen from Table 1 and Fig. 5a, the Mo/Ti and Mo/Al atomic ratios have exhibited a decreasing trend with increasing calcination temperature. At lower calcination temperatures, the Mo/Al atomic ratio is found to be more than that of Mo/Ti ratio. It is an established fact in the literature that the difference in the surface-free energies between molybdena and alumina (about  $0.65 \text{ N m}^{-1}$ ) is larger than that of molybdena and titania (about  $0.3 \text{ N m}^{-1}$ ) [54]. This means that when both titania and alumina surfaces are bare, molybdena interacts preferentially with alumina portion rather than with titania. It is also well known that isoelectric point or point of zero charge (IEP) of the support oxide also plays a decisive role in the extent of molybdate ion adsorption during preparation. As the isoelectric point of alumina (7.4–8.6) is much higher than that of titania (6.0–6.7), it suggests that the alumina surface should be more positively charged than titania surface and that molybdate adsorption should therefore occur preferentially on the alumina surface [55]. On the other hand, the concentration of anionic surface hydroxyl groups and their distribution on the surface is also the guiding factor for Mo distribution. Both the component oxides are known to have higher concentration of hydroxyl groups on their surfaces, but are uniformly distributed on the  $\text{TiO}_2$  surface [56] and in parallel rows on the  $\text{Al}_2\text{O}_3$  surface [57]. This inherent difference between  $\text{Al}_2\text{O}_3$  and  $\text{TiO}_2$  is reflected in a different distribution of Mo on alumina and titania regions of the mixed oxide support. As Mo is spread more uniformly on  $\text{TiO}_2$  than on  $\text{Al}_2\text{O}_3$  surface, it is expected that size of the monolayer patches may be lower on  $\text{TiO}_2$  than on alumina. Ng and Gulari [58] reported formation of multilayer patches and bulk  $\text{MoO}_3$  on  $\text{TiO}_2$  support when monolayer coverage is exceeded, while for the  $\text{Mo}/\text{Al}_2\text{O}_3$  system multilayer patches were formed even at submonolayer loadings. At higher temperatures, molybdena has less interaction with the support as a result of support sintering, thereby lowering the dispersion on the carrier surface. Another interesting observation from the quantification data is that at 1073 K, dispersion of molybdena was found to be more on titania than on alumina. The occurrence of the well-known and mobile  $\text{MoO}_2(\text{OH})_2$  species, which are formed by reaction of  $\text{MoO}_3$  and  $\text{H}_2\text{O}$  vapor at elevated temperatures [59], would facilitate the diffusion of Mo species into the octahedral interstices of  $\text{Al}_2\text{O}_3$  enhancing formation and growth



of  $\text{Al}_2(\text{MoO}_4)_3$  compound. The compound formation and its diffusion into the bulk may probably be the reason for the observed decrease in the Mo/Al than Mo/Ti at 1073 K.

#### 4. Conclusions

The following conclusions can be drawn from this study. (a) The core level binding energy of Al 2p increased with increasing calcination temperature. However, the magnitude of increase was slightly more in the case of molybdena-doped samples. This may be due to the removal of negative charge density by exchange of surface hydroxyls between the active component and the support oxide. (b) The presence of more titania than alumina lowers the interaction between molybdena and alumina, and results in a better resolution of Mo 3d doublet. (c) The Ti/Al ratio was found to decrease with increasing calcination temperature, which may be due to thermally-induced surface enrichment of alumina by concentration gradient. (d) The Mo/Al atomic ratio was found to be higher than that of Mo/Ti ratio, and both also decreased with increasing calcination temperature. The difference in the distribution of molybdena over the mixed oxide components is mainly due to various reasons, such as the difference in free energies, isoelectric point, and distribution of hydroxyl groups.

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