

# An XPS study of $\text{La}_2\text{O}_3$ and $\text{In}_2\text{O}_3$ influence on the physicochemical properties of $\text{MoO}_3/\text{TiO}_2$ catalysts

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## Abstract

To explore the influence of  $\text{La}_2\text{O}_3$  and  $\text{In}_2\text{O}_3$  doped  $\text{TiO}_2$  support on the dispersion and chemical nature of Mo-oxide species an investigation was undertaken by using XPS and other techniques. In this study, the  $\text{La}_2\text{O}_3\text{-TiO}_2$  and the  $\text{In}_2\text{O}_3\text{-TiO}_2$  binary oxide supports were prepared by a homogeneous coprecipitation method with in situ generated ammonium hydroxide and were deposited with  $\text{MoO}_3$  by adopting a wet impregnation technique. The Mo-containing catalysts and the corresponding supports were characterized by means of XRD, FTIR, XPS, and BET surface area methods. Characterization results suggest that the calcined (773 K)  $\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{In}_2\text{O}_3\text{-TiO}_2$  binary oxides are in X-ray amorphous state and exhibit reasonably high specific surface area. These supports also accommodate a monolayer equivalent of  $\text{MoO}_3$  (12 wt.%) in a highly dispersed state on the surface. Both  $\text{La}_2\text{O}_3$  and  $\text{In}_2\text{O}_3$  dopants show a strong influence on the electronic properties of the  $\text{MoO}_3/\text{TiO}_2$  catalysts as evidenced by a change in the XPS binding energies of these metal oxides. The XPS binding energy values further indicate that the dispersed molybdenum oxide is in Mo(VI) oxidation-state. However, the maximum broadening of Mo 3d as observed from full width at half-maximum values indicates that the presence of different Mo(VI) species on both the support surfaces. © 2001 Elsevier Science B.V. All rights reserved.

**Keywords:** Molybdenum oxide;  $\text{La}_2\text{O}_3\text{-TiO}_2$ ;  $\text{In}_2\text{O}_3\text{-TiO}_2$ ; Mixed oxide; Acid–base properties; X-ray diffraction; X-ray photoelectron spectroscopy; Dispersion

## 1. Introduction

Molybdena–titania catalysts are excellent for selective oxidation of hydrocarbons [1], ammoxidation of hetero-aromatic compounds [2], and selective catalytic reduction of  $\text{NO}_x$  with ammonia [3]. Moreover they are the precursors of alkene metathesis catalysts [4] and of sulfided hydrodesulfurization catalysts

[5,6]. It is an established fact in the literature that the activity and selectivity of the supported molybdenum catalysts is highly sensitive to the composition of the support and in the case of  $\text{TiO}_2$ -supported catalysts, the phase of support [7]. Eon et al. [8] have suggested that molybdena–titania interaction takes place through a perfect adjustment of (0 1 0) planes of  $\text{MoO}_3$  with (0 0 1) planes of  $\text{TiO}_2$ -anatase, thus leading to an epitaxial growth in the (0 1 0) direction of  $\text{MoO}_3$  crystals over the  $\text{TiO}_2$ . A high dispersion of octahedral polymolybdate over titania surface was reported by Ng and Gulari [9] by using laser Raman and IR spectroscopic methods. Other investigators

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employing ESR and other techniques have also supported these observations [10].

Oxidation reactions are playing an important role, both in the production of useful chemicals as well as in the destruction of undesired organics by total catalytic oxidation. Several efforts are being made in the literature on the one hand to develop various kinds of new catalysts to satisfy the needs for practical applications, and on the other hand, to explore the nature and structure of the active phase of the catalysts by employing several modern physicochemical techniques [11–14]. Recently, we have reported that the titania anatase structure can be stabilized even up to 1273 K with incorporation of other stable oxides such as  $\text{Al}_2\text{O}_3$ ,  $\text{SiO}_2$ , and  $\text{ZrO}_2$  and having vanadium or molybdenum oxides present as a monolayer on these mixed oxide surfaces [15–17]. In particular, the combined  $\text{V}_2\text{O}_5/\text{Ga}_2\text{O}_3\text{-TiO}_2$  catalyst was found to exhibit interesting catalytic activity for the selective oxidation of 4-methylanisole to anisaldehyde [18]. The  $\text{La}_2\text{O}_3$  is an important basic material and has been widely employed as a catalyst [19] and catalyst support [20], particularly in the oxidative coupling of methane (OCM). The lanthanum titanate catalyst activates methane more selectively than the individual oxides [19]. The  $\text{In}_2\text{O}_3$  is another interesting basic oxide, which has also often been used as a promoter in HZSM-5 zeolites for SCR of NO with  $\text{CH}_4$  in the presence of excess oxygen [21].

Over the past years, a great deal of fundamental and applied research work was focussed, especially, on supported molybdena catalysts because of their numerous applications in petroleum refining, chemicals production, and pollution control industries [1,5,9,11–15]. The Mo-oxide catalysts supported on conventional supports such as  $\text{Al}_2\text{O}_3$ ,  $\text{SiO}_2$  and  $\text{TiO}_2$  have been extensively investigated by a variety of techniques, conventional bulk sampling techniques as well as surface sensitive electron and ion spectroscopies, in an attempt to elucidate the nature of catalytic active surface species, and to study the coordination environment of the active metal center. The high surface sensitive photoelectron spectroscopy (XPS), is one of the best techniques to study the nature of Mo-oxide species on different supports.

In continuation to our earlier effort of making various kinds of mixed oxides possessing different acid–base characteristics [17,22], in this study, the

$\text{La}_2\text{O}_3\text{-TiO}_2$  and the  $\text{In}_2\text{O}_3\text{-TiO}_2$  binary oxides have been prepared, deposited with  $\text{MoO}_3$  by adopting a wet impregnation technique, and were investigated by XPS and other techniques. The primary goal of this study was to explore the influence of the surface structure of the support on the dispersion and chemical nature of Mo-oxide species.

## 2. Experimental methods

### 2.1. Catalyst preparation

The  $\text{La}_2\text{O}_3\text{-TiO}_2$  (1:5 molar ratio) and  $\text{In}_2\text{O}_3\text{-TiO}_2$  (1:13 molar ratio) binary oxides were prepared by a co-precipitation method where ammonia was generated in situ by decomposition of urea at 363 K [23]. In a typical experiment, the required quantities of titanium tetrachloride (Fluka, AR grade) and lanthanum nitrate (Loba, GR grade) or indium chloride (Aldrich, AR grade), dissolved separately in deionized water were mixed together. Cold  $\text{TiCl}_4$  was first digested in cold concentrated HCl and subsequently diluted with deionized water. In the case of  $\text{In}_2\text{O}_3\text{-TiO}_2$  mixed oxide, the indium chloride precursor was dissolved in an excess solution of ethanol. An excess amount of solid urea with a metal to urea molar ratio of 1:2.5 was also added to the mixture solution. The resulting mixture was heated slowly to 363–368 K on a hot plate with vigorous stirring. The pH of the solution was monitored at different intervals of time. No change in the pH of the solution was observed until the temperature reached to 363–368 K. At this temperature the pH of the solution increased slowly in the beginning from 3.5 to 4.5 and rapidly with increase in the time of heating, attaining a final value between 7 and 8. Heating was further continued at this temperature for 6 h in order to complete the precipitation. The resulting precipitates were filtered, washed with deionized water until no chlorides could be detected with  $\text{AgNO}_3$  in the filtrate. The resulting cake was then oven dried at 383 K for 12 h and finally calcined at 773 K for 6 h in air atmosphere. A nominal 12 wt.%  $\text{MoO}_3$  was deposited on the calcined mixed oxides by adopting a wet impregnation method [15]. To impregnate  $\text{MoO}_3$  the calculated amount of ammonium heptamolybdate (J.T. Baker, UK, AR grade) was dissolved in doubly distilled water and a few drops of dilute  $\text{NH}_4\text{OH}$  was

added to make the solution clear and to keep the pH constant (pH 8). Finely powdered calcined (773 K) supports were then added to this solution and the excess water was evaporated on a water-bath with continuous stirring. The resultant solid was then dried at 383 K for 12 h and calcined at 773 K for 5 h in the flow of oxygen ( $40 \text{ cm}^3 \text{ min}^{-1}$ ). The rate of heating (as well as cooling) was always maintained at  $10 \text{ K min}^{-1}$ .

## 2.2. Catalyst characterization

X-ray diffraction analysis was performed on a Siemens D-5000 diffractometer by using Cu  $K\alpha$  radiation source and Scintillation Counter detector. The XRD phases present in the samples were identified with the help of ASTM Powder Data Files. The BET surface area of the samples was determined by  $\text{N}_2$  physisorption at 77 K by taking  $0.162 \text{ nm}^2$  as the area of cross section of  $\text{N}_2$  molecule.

The XPS measurements were made on a VG scientific ESCA Lab II Spectrometer (resolution 0.1 eV) with Mg  $K\alpha$  (1253.6 eV) radiation as the excitation source [16]. Before experiments the spectrometer was calibrated against  $\text{Eb}(\text{Au } 4f_{7/2}) = 84.0 \text{ eV}$  and  $\text{Eb}(\text{Cu } 2p_{3/2}) = 932.6 \text{ eV}$  [24]. The C 1s line was taken as internal reference with a binding energy of 285.0 eV [24]. An estimated error of  $+0.1 \text{ eV}$  can be assumed for all the measurements. The finely ground oven dried samples were mounted on the standard sample holder and covered by a gold mask. The sample holder was then fixed on a rod attached to the pretreatment chamber. Before transferring them to the main chamber the samples were degassed ( $1 \times 10^{-7}$  Torr) in the pretreatment chamber overnight at room temperature. The degassed samples were then transferred into the main chamber and the XPS analysis was done at room temperature and pressures typically less than  $10^{-8}$  Torr [24].

## 3. Results and discussion

X-ray powder diffraction patterns of  $\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{In}_2\text{O}_3\text{-TiO}_2$  supports along with their corresponding  $\text{MoO}_3$  containing catalysts are shown in Fig. 1. As can be noted, the lanthana–titania binary oxide is in X-ray amorphous state with broad background diffraction lines due to a poorly crystalline  $\text{TiO}_2$

anatase phase (JCPDS Files no. 21-1272). However, in the case of  $\text{In}_2\text{O}_3\text{-TiO}_2$  sample, a few characteristic  $\text{TiO}_2$ -anatase lines can be seen indicating that this material is in a slightly crystalline form than that of  $\text{La}_2\text{O}_3\text{-TiO}_2$ . It can also be noted from Fig. 1 that in both the cases that there is no evidence of any specific compound formation between  $\text{La}_2\text{O}_3$  or  $\text{In}_2\text{O}_3$  and  $\text{TiO}_2$ . The FTIR spectra of these samples also supported the XRD observations indicating that there is no evidence of the formation of oxide compounds of lanthanum or indium with titanium when calcined at 773 K. The  $\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$  is also in X-ray amorphous state with broad background lines due to  $\text{TiO}_2$ -anatase phase, whereas the  $\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$  catalyst exhibits a few characteristic  $\text{TiO}_2$ -anatase lines. Very interestingly, no XRD lines due to crystalline  $\text{MoO}_3$  or  $\text{TiO}_2$ -rutile phases were observed in both cases. This observation indicates that the impregnated molybdenum oxide is in a highly dispersed state or the crystallites formed are less than the detection capability of the XRD technique. The 12 wt.% loading of  $\text{MoO}_3$  corresponds to the monolayer capacities of these oxides and supports the former possibility [25]. The FTIR spectra of these samples also supported the XRD observations. Anatase phase of titania normally exhibits strong absorption bands at  $676$  and  $547 \text{ cm}^{-1}$  and the rutile phase at  $660$  and  $455 \text{ cm}^{-1}$ , respectively [26]. The presence of these bands due to  $\text{TiO}_2$ -anatase phase is noted for both series of samples. Generally, the IR band of  $\text{Mo=O}$  in crystalline  $\text{MoO}_3$  appears at  $1000 \text{ cm}^{-1}$  due to the stretching vibration mode [15,26,27]. Irrespective of the support, no characteristic bands due to crystalline  $\text{MoO}_3$  were observed which indicates clearly that the molybdenum oxide is in a highly dispersed state on the support. As shown in Table 1, both supports show reasonably high specific surface areas. After impregnation with  $\text{MoO}_3$  a small decrease in the specific surface area of the samples can be noted. This is primarily due to a high dispersion of molybdenum oxide in the pores of the support [15]. The  $\text{O}_2$  chemisorption measurements as per the procedure described elsewhere [15] also reveal that the impregnated molybdenum oxide is in a highly dispersed state on both support surfaces. This method nicely discriminates between the dispersed state and the crystalline molybdenum oxide phase.

The  $\text{La}_2\text{O}_3\text{-TiO}_2$ ,  $\text{In}_2\text{O}_3\text{-TiO}_2$ ,  $\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$  samples were investigated by

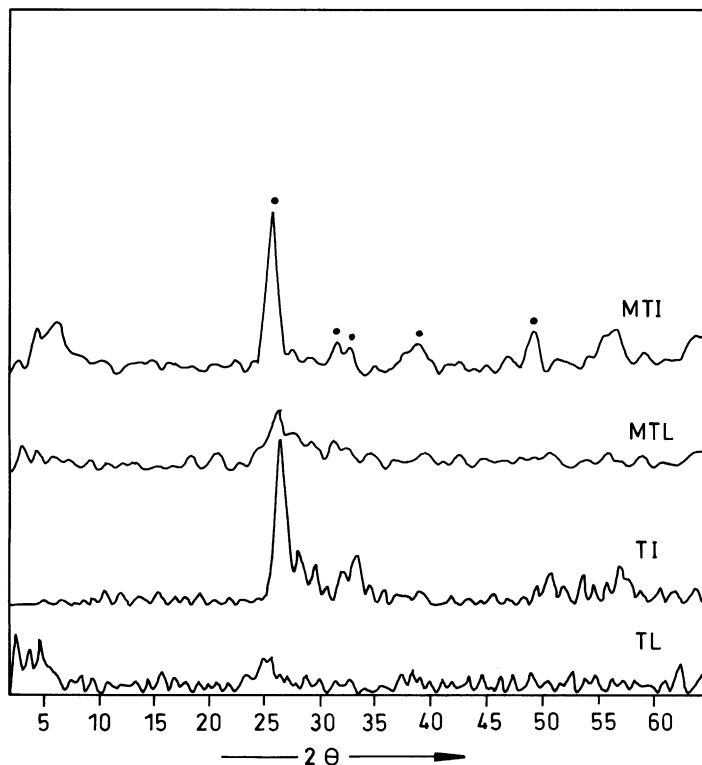


Fig. 1. X-ray powder diffraction patterns of  $\text{La}_2\text{O}_3\text{-TiO}_2$ ,  $\text{In}_2\text{O}_3\text{-TiO}_2$ ,  $\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$  samples calcined at 773 K. (●) Lines due to  $\text{TiO}_2$ -anatase phase.

Table 1

Composition, BET surface area and XRD phase composition of the samples investigated in this study

Sample	Support composition (mole ratio)	BET SA ( $\text{m}^2 \text{g}^{-1}$ )	XRD phases observed
$\text{La}_2\text{O}_3\text{-TiO}_2$	1:5	132	Amorphous
$\text{In}_2\text{O}_3\text{-TiO}_2$	1:13	125	$\text{TiO}_2$ -anatase
$\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$	1:5	96	Amorphous
$\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$	1:13	115	$\text{TiO}_2$ -anatase

XPS technique. The representative XPS bands of O 1s, Ti 2p together with In 3d, La 3d, and Mo 3d without smoothing are shown in Figs. 2–5, respectively, and the corresponding binding energies and full width at half maximum (FWHM) values are summarized in Table 2. For the purpose of better comparison, the XPS bands of O 1s and Ti 2p along with In 3d pertaining to the supports are shown in Figs. 2a and 3a, respectively, and the corresponding bands of  $\text{MoO}_3$  containing catalysts are shown in Figs. 2b and 3b,

respectively. These figures and Table 2 clearly indicate that the XPS bands are highly sensitive to the composition of the mixed oxide support and also the presence of  $\text{MoO}_3$  on these carriers.

The O 1s profile, as presented in Fig. 2, is complicated due to the overlapping contribution of oxygen from both individual oxides as well as from  $\text{MoO}_3$  in the case of Mo-containing catalysts. As reported in the literature [24,28], the O 1s binding energy of pure  $\text{TiO}_2$  is 530.1 eV. However, a small lowering of the

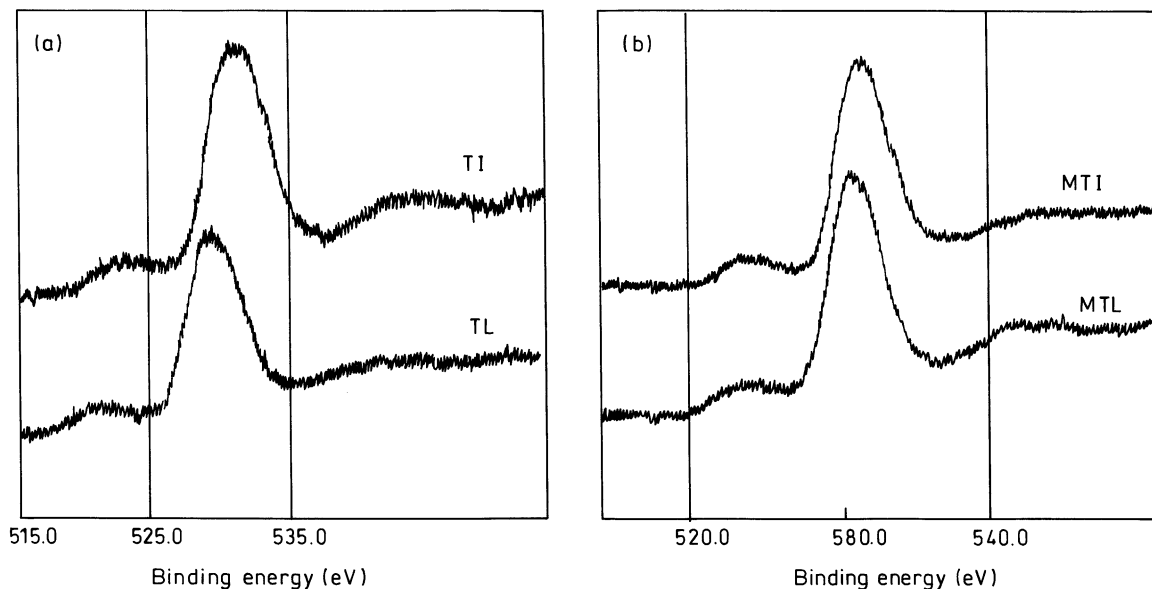


Fig. 2. XPS of the O 1s region for  $\text{La}_2\text{O}_3\text{-TiO}_2$ ,  $\text{In}_2\text{O}_3\text{-TiO}_2$ ,  $\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$  samples calcined at 773 K.

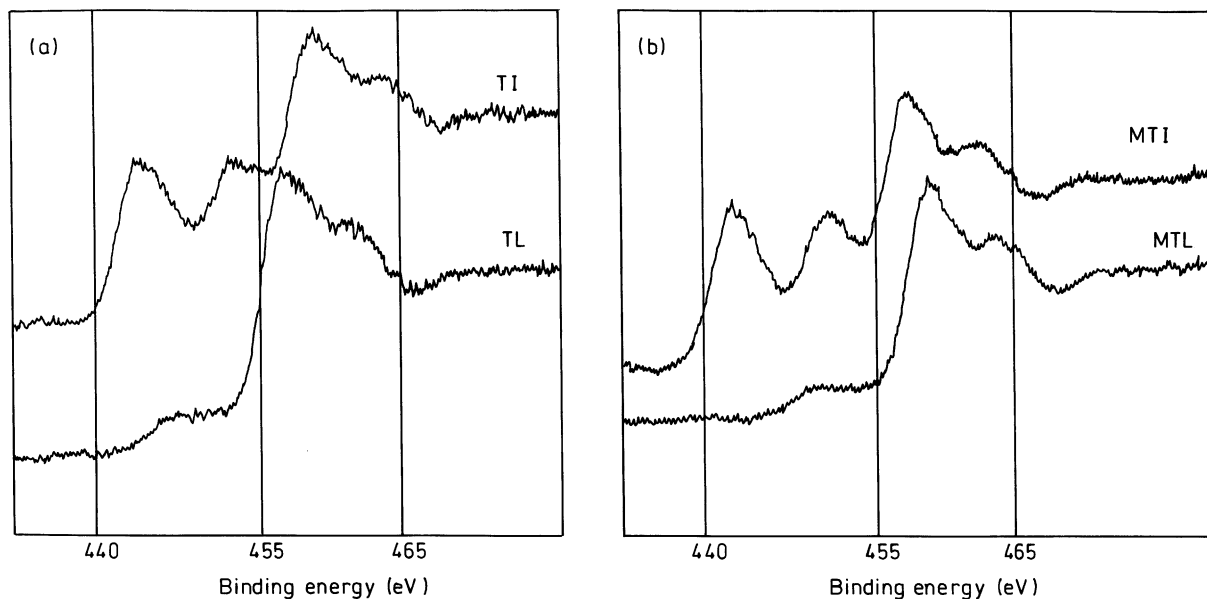


Fig. 3. (a) Ti 2p and In 3d XPS binding energy region for  $\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{In}_2\text{O}_3\text{-TiO}_2$  samples. (b) Ti 2p and In 3d XPS binding energy region for  $\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$  samples.

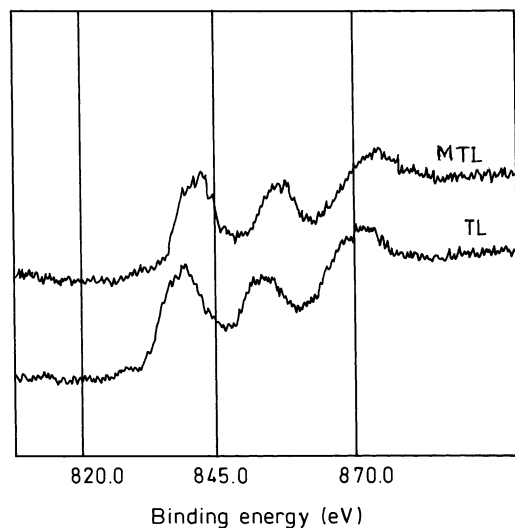


Fig. 4. La 3d XPS spectra of  $\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$  samples calcined at 773 K.

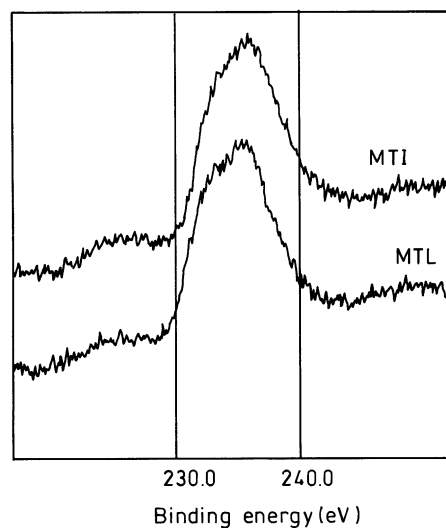


Fig. 5. Mo 3d XPS spectra of  $\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$  samples calcined at 773 K.

O 1s binding energy can be noted for  $\text{La}_2\text{O}_3\text{-TiO}_2$  sample as well as for Mo-containing catalysts.

Fig. 3 shows the binding energies of Ti 2p photoelectron peaks at around 458.0 and 464.0 eV for Ti  $2p_{3/2}$  and Ti  $2p_{1/2}$  lines, respectively. As In 3d core level binding energy value (444.6 eV for pure  $\text{In}_2\text{O}_3$  [29]) is closer to Ti 2p binding energy values, therefore, both have been recorded in the same range and presented in Fig. 3. As shown in Table 2, the Ti  $2p_{3/2}$  binding energy of the  $\text{La}_2\text{O}_3\text{-TiO}_2$  mixed oxide was found to be 457.0 eV, which is lower than that of the pure  $\text{TiO}_2$  (458.0 eV) [30]. The Pauling electronegativity value of Ti is 1.5 and of La is 1.1 [31], which indicates the possibility of electron transfer from lanthanum to titanium in the Ti–O–La bond. This charge transfer makes Ti more electron rich and lowers the Ti  $2p_{3/2}$  core electron binding energy. Moreover, the binding energy value for La 3d also decreases for

$\text{La}_2\text{O}_3$  in the mixed oxide as compared to the value found at 834.8 eV for pure lanthanum oxide [24]. In the case of  $\text{In}_2\text{O}_3\text{-TiO}_2$  sample, the core level binding energy of Ti 2p was found to be 459.0 eV, which is more than that of pure titania. It can be interpreted again from the Pauling electronegativity values of the corresponding elements. Pauling E.N. value for indium is 1.7, which is more than that of titania thus favoring negative charge transfer towards indium in the Ti–O–In bond thereby increasing Ti 2p core level binding energy. The binding energy value of In 3d in the mixed oxide remains the same with that found in the literature [32,33] for pure indium oxide. Substitution of  $\text{In}^{3+}$  in the titania matrix generates an excess negative charge around these elements due to non-stoichiometric oxide ion. Therefore, the corresponding binding energy of In 3d remains the same in the mixed oxides.

Table 2

XPS binding energies and FWHM values of binary oxide supports and  $\text{MoO}_3$  containing catalysts

Sample	O 1s (eV)	Ti $2p_{3/2}$ (eV)	La 3d (eV)	In 3d (eV)	Mo 3d (eV)	FWHM (eV)
$\text{La}_2\text{O}_3\text{-TiO}_2$	529.0	457.0	833.0	–	–	–
$\text{In}_2\text{O}_3\text{-TiO}_2$	530.0	459.0	–	444.5	–	–
$\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$	529.5	458.5	834.0	–	235.0	7.5
$\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$	529.5	457.5	–	443.0	234.0	8.0

The binding energy values of La 3d and In 3d for  $\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$ , respectively, was decreased when compared to the values found for the corresponding pure oxides [24,29]. The explanation is that because of strong interaction between the acidic  $\text{MoO}_3$  and basic  $\text{La}_2\text{O}_3$  and  $\text{In}_2\text{O}_3$  oxides there is strong shift in the BE values of the corresponding oxides when compared to the pure supports. The same was also responsible for the broadening of Mo 3d line.

Fig. 4 presents the XPS patterns of La 3d levels before and after impregnating with  $\text{MoO}_3$ . Apart from La 3d doublet at around 834.8 eV, a third peak in the figure is due to the auger emission from titanium atom [34]. The Mo  $3d_{5/2}$  photoelectron peak of  $\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$  catalysts is shown in Fig. 5. The binding energy values presented in Table 2 indicate the presence of Mo(VI) species on both support surfaces [35]. The FWHM values shown in Table 2 indicate clearly the presence of different molybdena species on both support surfaces as envisaged earlier [22,36]. The Mo 3d doublet was well resolved in the case of  $\text{MoO}_3/\text{TiO}_2\text{-ZrO}_2$  and  $\text{MoO}_3/\text{TiO}_2\text{-SiO}_2$  samples and a maximum peak broadening was noted in the case of  $\text{MoO}_3/\text{TiO}_2\text{-Al}_2\text{O}_3$  samples [22]. The literature reveals that the resolution of the doublet peak is quite poorer for  $\text{MoO}_3/\text{Al}_2\text{O}_3$  catalyst and improves considerably as one passes from Mo/ $\text{SiO}_2$  to Mo/ $\text{ZrO}_2$  to Mo/ $\text{TiO}_2$  systems [36]. The broadening of ESCA peak has been attributed to various factors including (1) the presence of more than one type of Mo(VI) with different chemical characteristics which cannot be discerned by ESCA [36,37], and (2) electron transfer between the active component and the support (metal–support interaction). At monolayer coverage the structure of surface molybdenum oxide species primarily possesses an octahedral coordination on  $\text{TiO}_2$  and a mixture of tetrahedral and octahedral coordination on  $\text{Al}_2\text{O}_3$  surface. A maximum Mo 3d peak broadening observed in the case of  $\text{MoO}_3/\text{TiO}_2\text{-Al}_2\text{O}_3$  sample was attributed to the existence of different octahedral and tetrahedral Mo species on this mixed oxide surface. The same analogy can be extended to the present catalyst systems where a similar Mo 3d broadening is noted. In particular, the  $\text{La}_2\text{O}_3$  and  $\text{In}_2\text{O}_3$  oxides in  $\text{TiO}_2$  show a strong influence on the chemical state of molybdenum when compared to other additives such

as  $\text{Al}_2\text{O}_3$ ,  $\text{SiO}_2$  and  $\text{ZrO}_2$ . This is primarily due a strong acid–base interaction between the basic  $\text{La}_2\text{O}_3$  and  $\text{In}_2\text{O}_3$  oxides and the acidic  $\text{MoO}_3$ .

It is an established fact in the literature that the nature of the surface molybdenum oxide species formation in a supported catalyst system mainly depends (i) on the nature and number of OH groups present on the support; (ii) mode of binding of Mo oxide precursors to OH groups during impregnation; and (iii) transformation of surface species during drying and calcination. The  $\text{NH}_4^+$  ions are removed during calcination and the  $\text{H}^+$  ion coordinate to the surface molybdenum oxide species in order to compensate for the net charge. Therefore, the molecular structures of the surface molybdenum oxide species of the calcined samples are mainly dependent on the net surface pH at point of zero charge (PZC) [38]. The oxide supports with low pH at PZC such as  $\text{SiO}_2$  (pH at PZC = 1.8–3.9) were found to favor the octahedrally coordinated polymolybdate species such as  $\text{Mo}_8\text{O}_{26}^{4-}$  and/or  $\text{Mo}_7\text{O}_{24}^{6-}$ . On the other hand, the amphoteric oxide supports,  $\text{TiO}_2$  (anatase, pH at PZC = 6.2) and  $\text{ZrO}_2$  (pH at PZC = 6.7), favor the formation of same octahedrally coordinated polymolybdate species. The  $\text{Al}_2\text{O}_3$  support (pH at PZC 6.0–8.9) possesses both monomeric ( $\text{MoO}_4^{2-}$ ) and polymeric species ( $\text{Mo}_7\text{O}_{24}^{6-}$ ) at high pH values. Presence of basic  $\text{La}_2\text{O}_3$  and  $\text{In}_2\text{O}_3$  oxides in the  $\text{TiO}_2$  support is expected to increase its pH at PZC. Therefore, different surface molybdena species are expected to be formed in conformity with the XPS observations.

#### 4. Conclusions

The following conclusions can be drawn from this study: (1) The  $\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{In}_2\text{O}_3\text{-TiO}_2$  binary oxides are interesting and promising support materials for the dispersion of molybdenum oxide. These calcined (773 K) mixed oxides are in X-ray amorphous state with broad diffraction lines due  $\text{TiO}_2$ -anatase phase and exhibit a high specific surface area. (2) The  $\text{MoO}_3/\text{La}_2\text{O}_3\text{-TiO}_2$  and  $\text{MoO}_3/\text{In}_2\text{O}_3\text{-TiO}_2$  catalysts calcined at 773 K also retain the  $\text{TiO}_2$ -anatase phase of the support and the impregnated molybdenum oxide being in a highly dispersed state. (3) Both  $\text{La}_2\text{O}_3$  and  $\text{In}_2\text{O}_3$  dopants show a strong influence on the chemical

properties of the  $\text{MoO}_3/\text{TiO}_2$  catalyst as evidenced by a change in the XPS binding energies. (4) The XPS binding energy values indicate that the dispersed molybdenum oxide is in Mo(VI) oxidation-state. However, the maximum broadening of Mo 3d as observed from FWHM values indicate the presence of different Mo(VI) species on both the supports.

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